

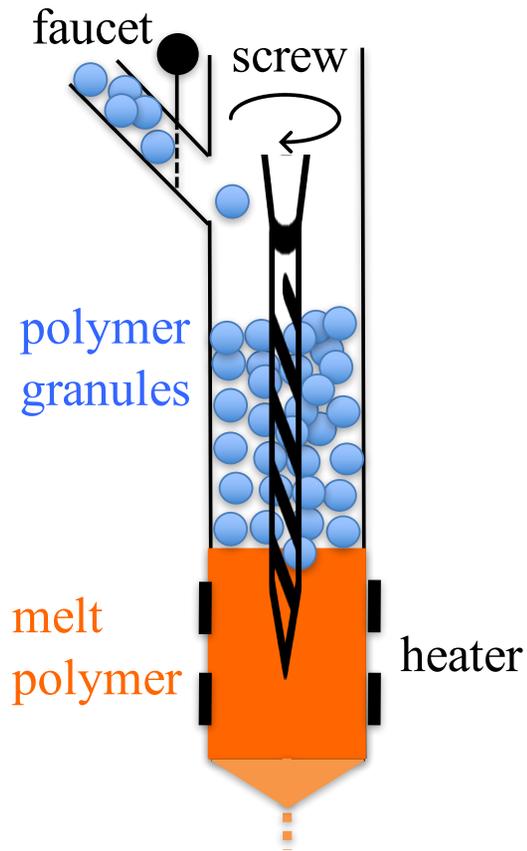
ISS for Control of Stefan Problem w.r.t Heat Loss at Interface

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Motivation : Screw Extruder for Polymer 3D Printing

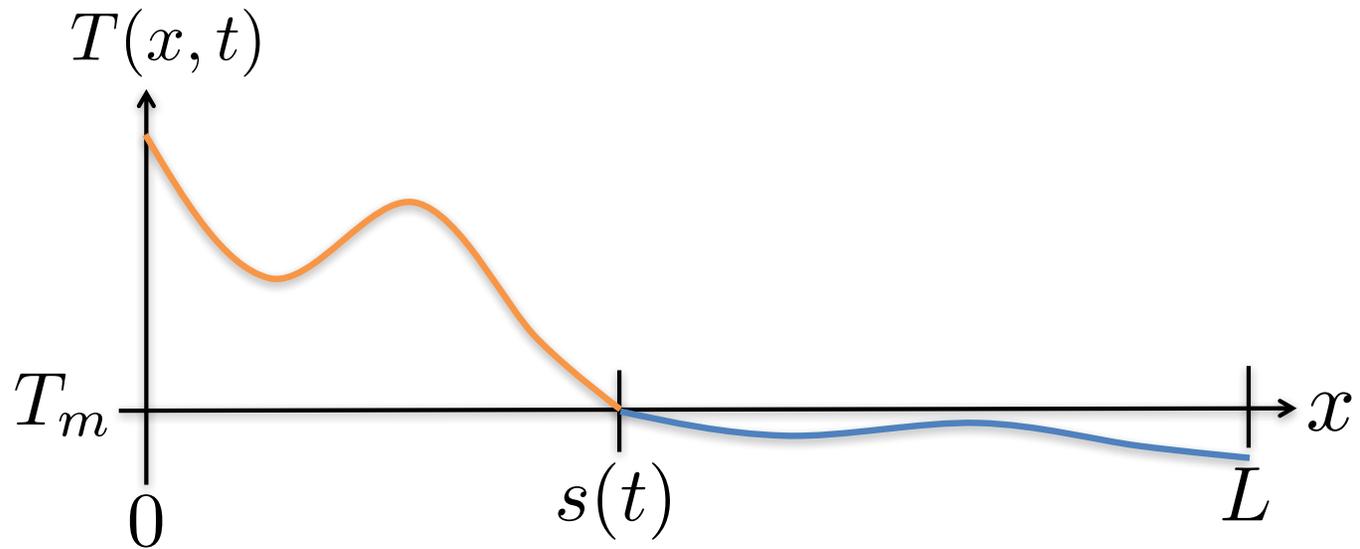
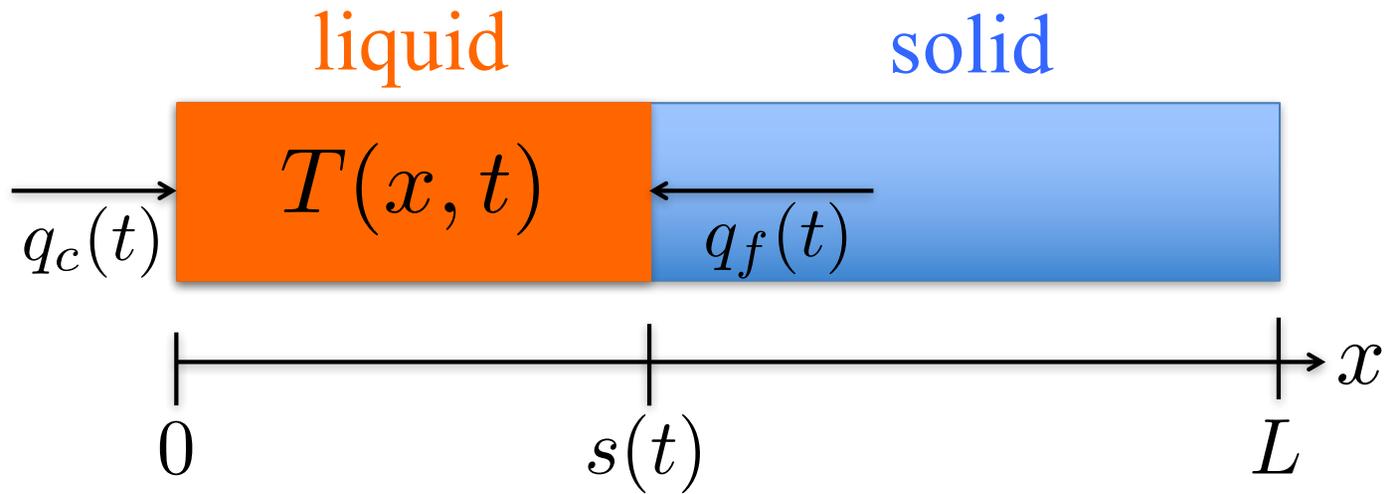


Model : Thermal phase change (melting/solidification)

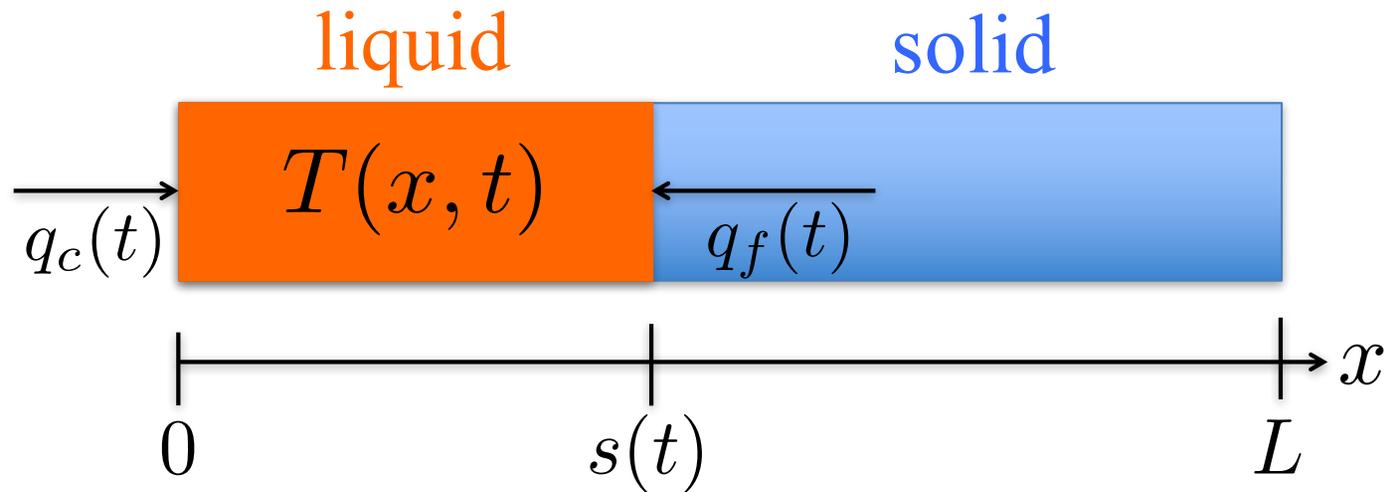
Objective : Stabilize ratio of granules/melt polymer

Property : Temperature in both phases are dynamic

Simplified Model : Melting + Heat Loss



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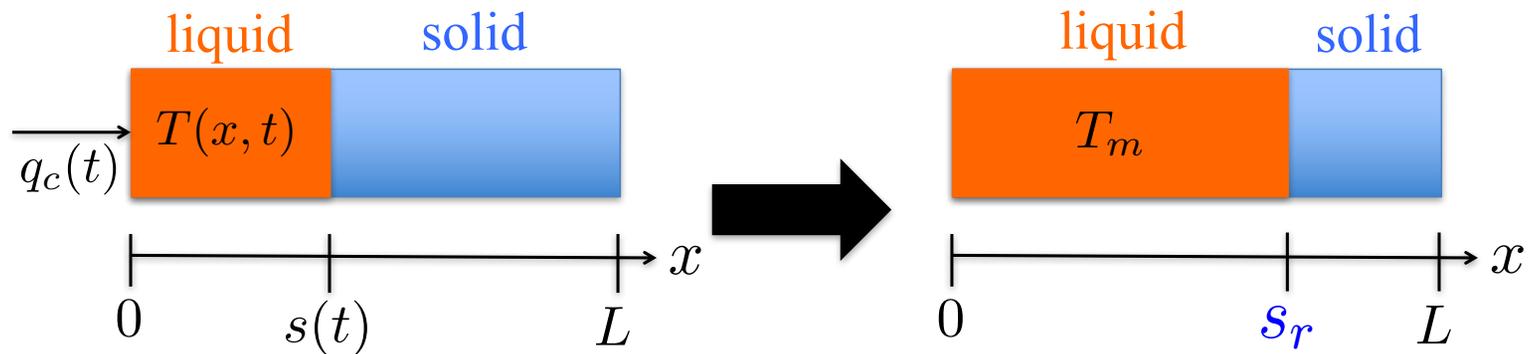
States : Temperature profile $T(x, t)$, Interface position $s(t)$

Control : Melting heat $q_c(t) > 0$

Disturbance : Freezing heat $q_f(t) > 0$ (magnitude) from solid phase

Problem

Previous work (ACC16) : Designed $q_c(t) > 0$ (feedback w.r.t. $T(x, t), s(t)$) to achieve $s(t) \rightarrow s_r$ under $q_f(t) \equiv 0$.



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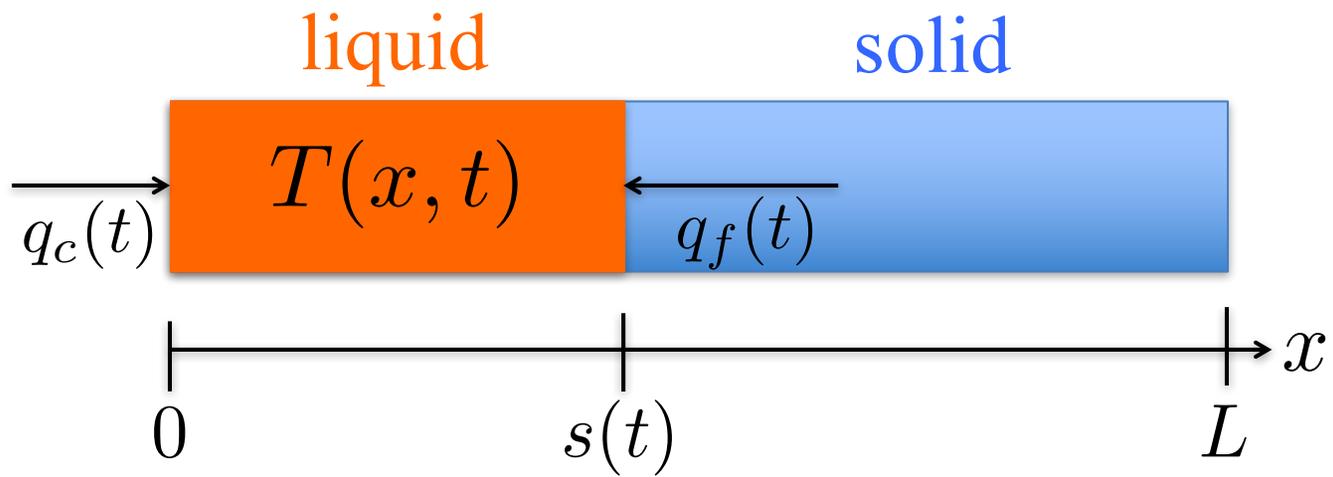
Question : What if there exists $q_f(t) \geq 0$? (under *same control design*)

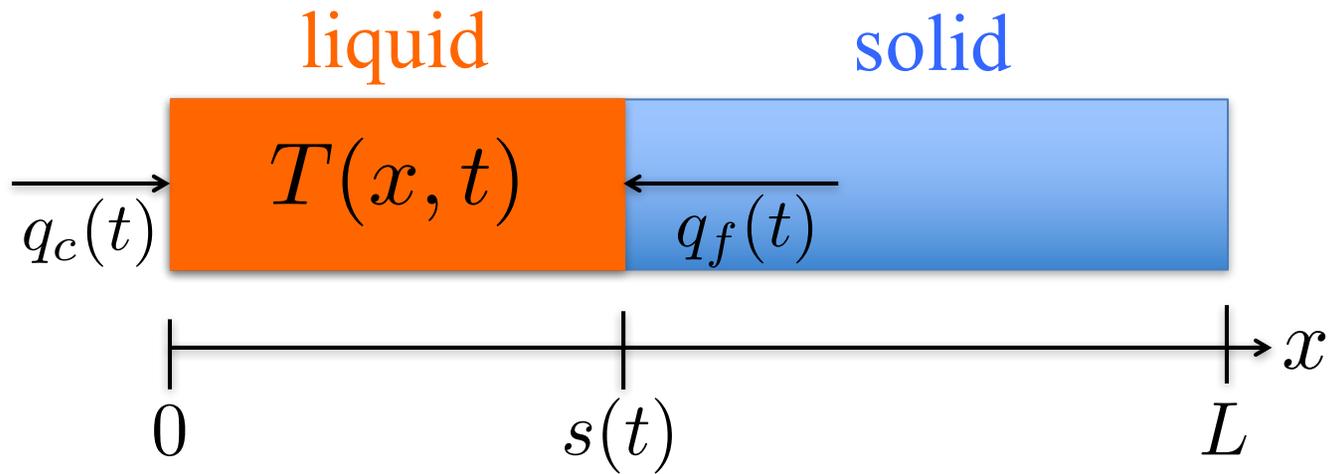
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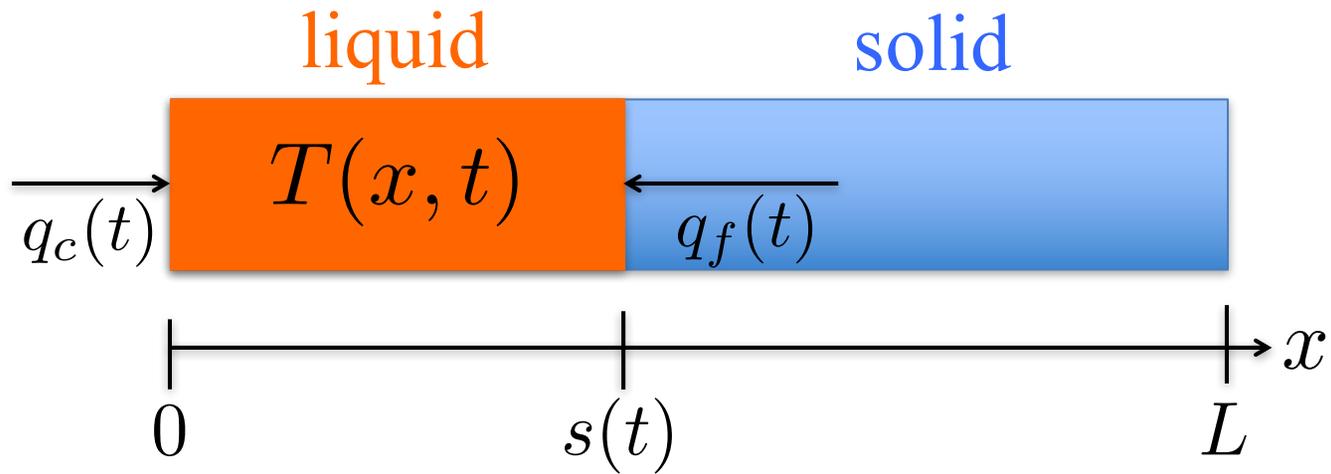
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→ Prove Input-to-State Stability (ISS) w.r.t. $q_f(t)$





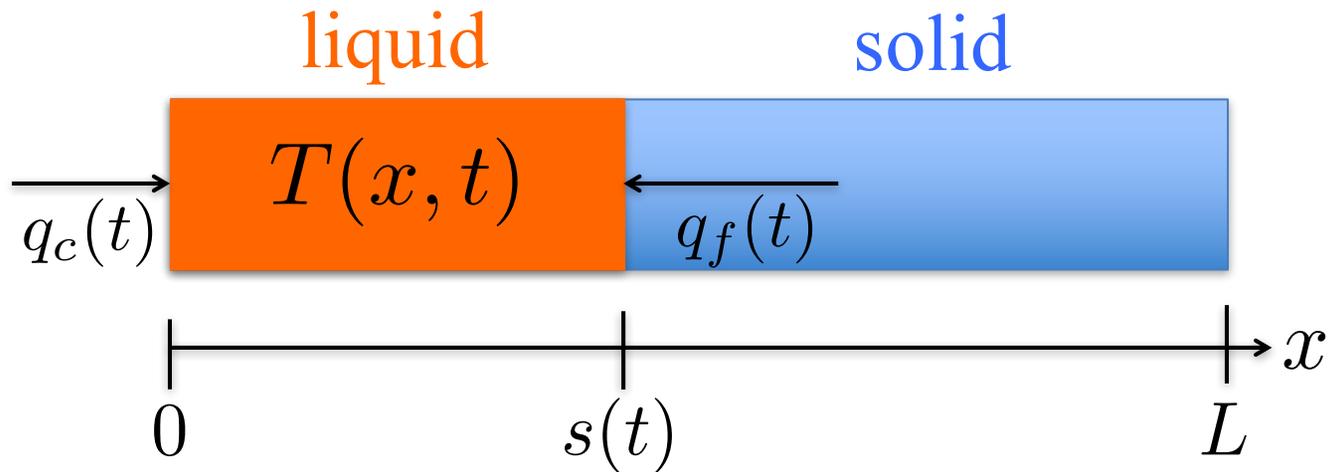
PDE $T_t(x, t) = \alpha T_{xx}(x, t), \quad 0 < x < s(t) < L$



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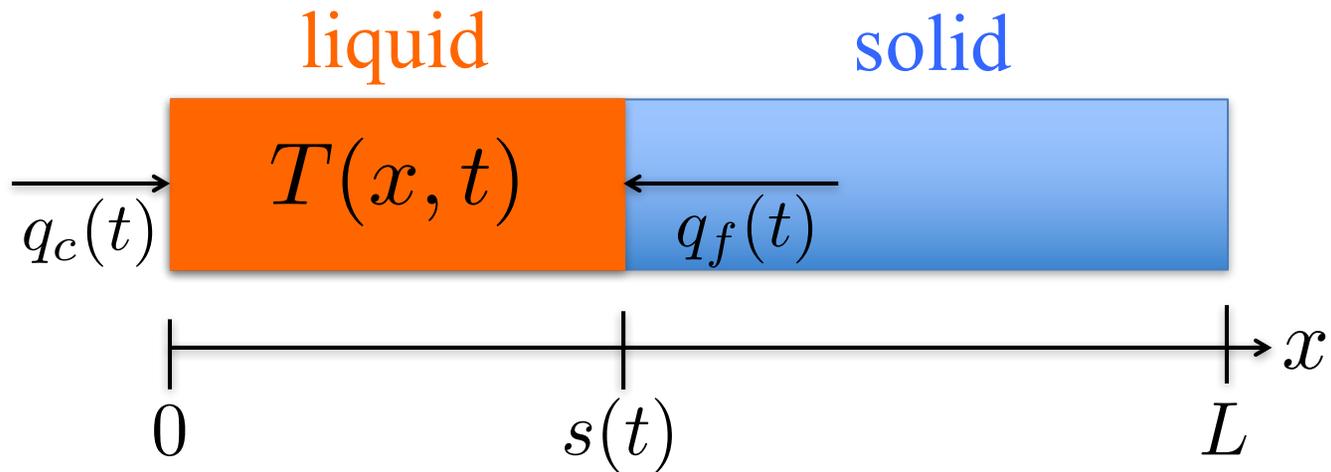


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State-dependent moving boundary \Rightarrow Nonlinear

Model valid iff

$$T(x, t) > T_m, \quad \text{for } \forall x \in (0, s(t)), \quad \forall t > 0$$

$$0 < s(t) < L, \quad \forall t > 0$$

Lemma If $q_c(t) > 0 \quad \forall t > 0$, then $T(x, t) > T_m, \quad \forall x \in (0, s(t)), \forall t > 0$

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Lemma If $q_c(t) > 0 \forall t > 0$, then $T(x, t) > T_m, \forall x \in (0, s(t)), \forall t > 0$

* $q_c(t) > 0$ and $0 < s(t) < L$ are proved after $q_c(t)$ is designed

Without heat loss ($q_f(t) \equiv 0$), the following assumption **necessary**

Assumption : Setpoint s_r chosen to satisfy

$$s_0 + \frac{\beta}{\alpha} \int_0^{s_0} (T_0(x) - T_m) dx < s_r < L$$

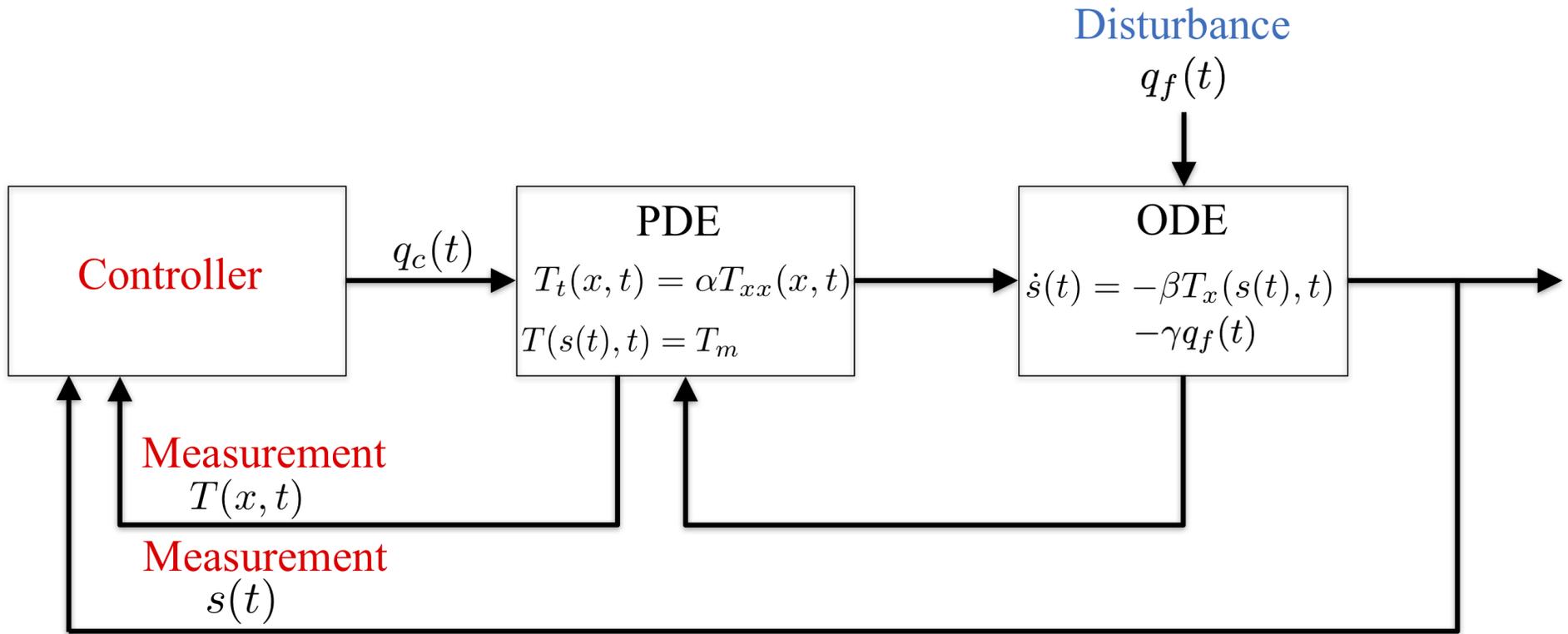
We impose the same assumption because $q_f(t)$ is an *unknown* disturbance.

Assumption : The heat loss is bounded and its total energy is also bounded, i.e.,
 $\exists \bar{q}_f, M > 0$ s.t.

$$0 \leq q_f(t) \leq \bar{q}_f$$

,

$$\int_0^{\infty} q_f(t) dt \leq M$$



Previous Result (ACC16) For $q_f(t) \equiv 0$, the control law

$$q_c(t) = -c \left(\frac{k}{\alpha} \int_0^{s(t)} (T(x, t) - T_m) dx + \frac{k}{\beta} (s(t) - s_r) \right)$$

where $c > 0$, makes the closed-loop system **globally exponentially stable** in the norm $\Psi(t) = \|T - T_m\|_{\mathcal{H}_1}^2 + (s - s_r)^2$.

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Theorem (ACC18) For $q_f(t) \geq 0$, the same control law with gain c satisfying $c > \frac{\beta}{k s_r} \bar{q}_f$, makes the closed-loop system **ISS w.r.t. $q_f(t)$** in the norm $\Psi(t) = \|T - T_m\|_{\mathcal{L}_2}^2 + (s - s_r)^2$.

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Note : Gain should be large to avoid complete frozen

Design Procedure

- Reference errors

$$u(x, t) := T(x, t) - T_m, \quad X(t) := s(t) - s_r$$

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$$w(x, t) = u(x, t) - \frac{\beta}{\alpha} \int_x^{s(t)} \phi(x - y) u(y, t) dy - \phi(x - s(t)) X(t)$$
$$\phi(x) = \frac{c}{\beta} x - \varepsilon$$

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- Target system ($d(t) := \gamma q_f(t)$)

$$w_t(x, t) = \alpha w_{xx}(x, t) + \dot{s}(t) \phi'(x - s(t)) X(t) + \phi(x - s(t)) d(t),$$

$$w(s(t), t) = \varepsilon X(t) \quad w_x(0, t) = \frac{\beta}{\alpha} \phi(0) u(0)$$

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→ Stable if $d(t) \equiv 0$.

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★ The controller is derived by transformation & target system

Analysis

Lemma The closed-loop satisfies $q_c(t) > 0$ and $0 < s(t) < L$

Lemma Target (w, X) -system is ISS w.r.t. $d(t)$

Proof is by ISS Lyapunov function. Define

$$V = \frac{1}{2\alpha} \|w\|_{L_2}^2 + \frac{\varepsilon}{2\beta} X^2$$

and derive

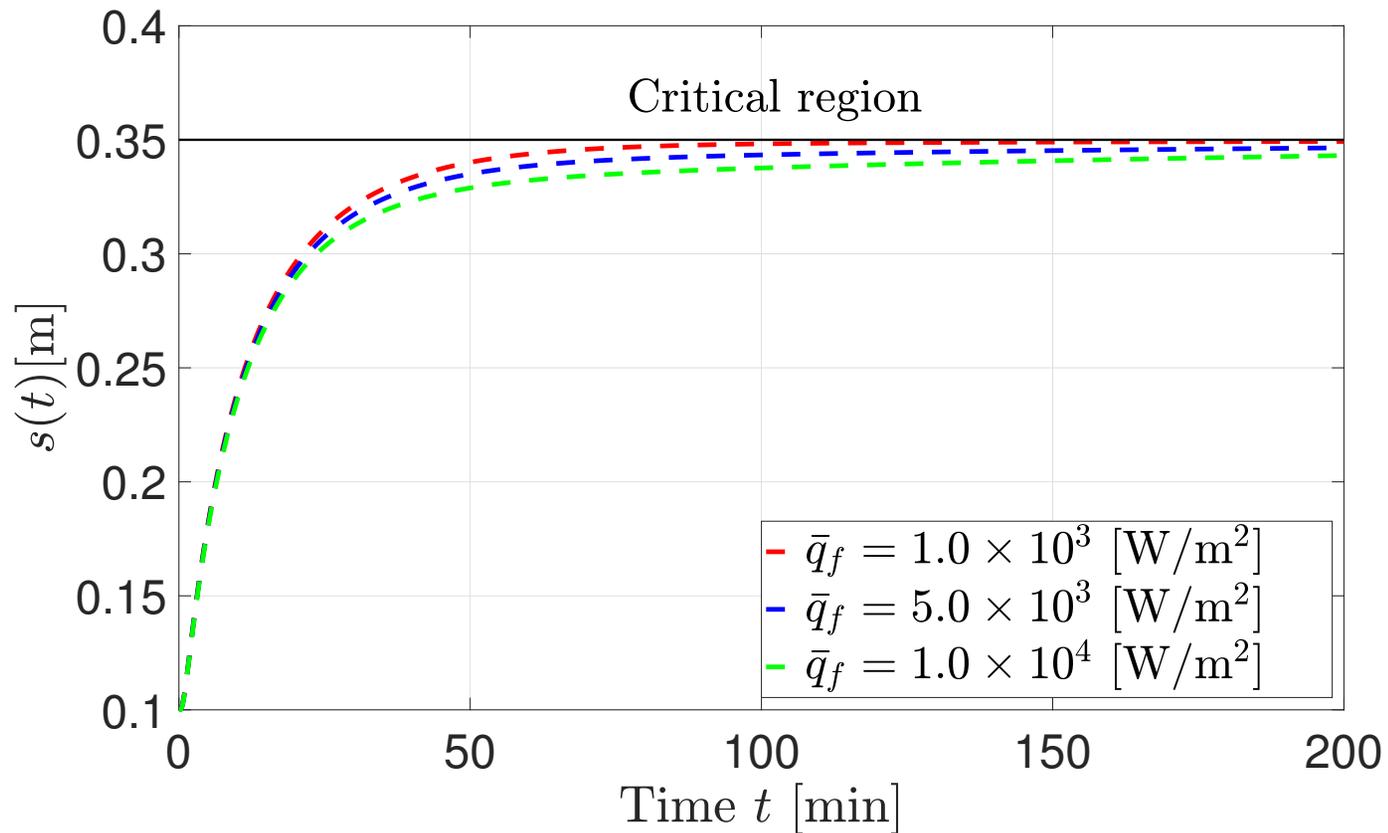
$$V(t) \leq M_1 V_0 e^{-bt} + M_2 \int_0^t e^{-b(t-\tau)} d(\tau)^2 d\tau$$

\Rightarrow concludes ISS of (T, s) at (T_m, s_r) w.r.t q_f .

Numerical Simulation

Zinc

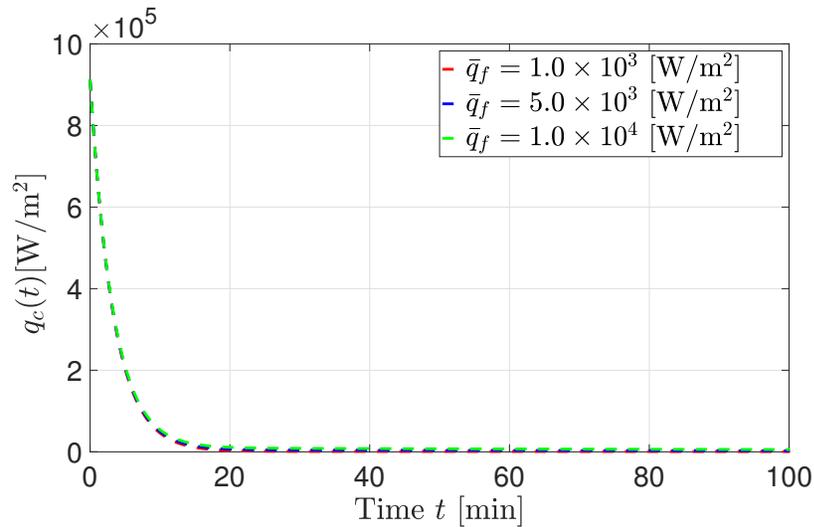
Heat loss $q_f(t) = \bar{q}_f e^{-Kt}$ with K extremely small (half life 40 [hour])



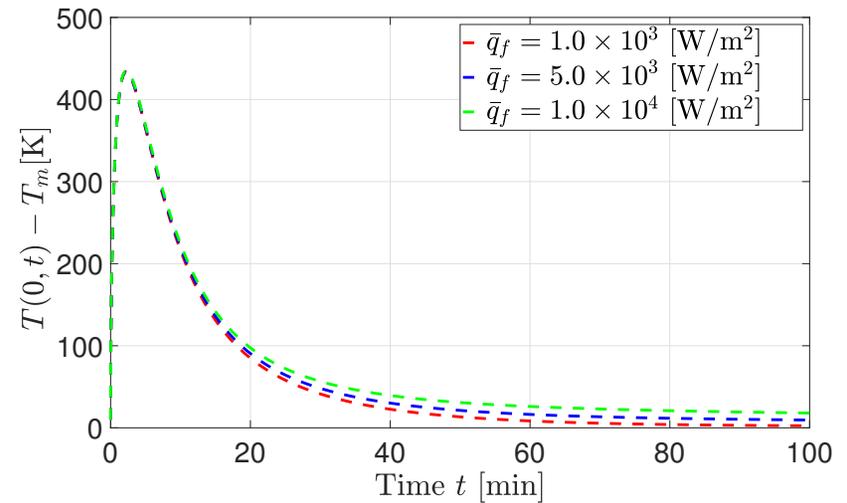
⇒ illustrates ISS property with $0 < s(t) < s_r$.

Numerical Simulation

Zinc



★ heat input maintains positive,

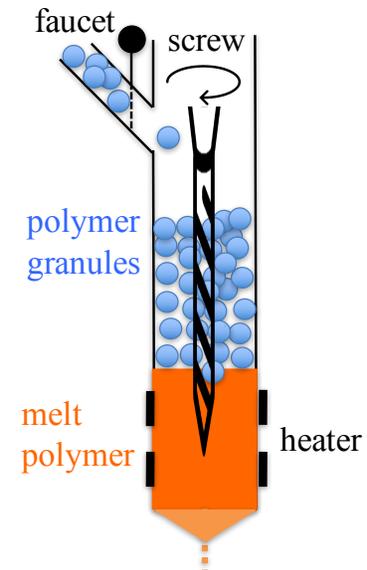


★ liquid temperature is above melting temperature

Future Work

- Incorporate screw extruder's dynamics

$$T_t = \alpha T_{xx} - bT_x - h(T - T_b)$$



- Redesign by two-phase temperature dynamics (CDC 2017)